



South Coast  
AQMD

# Proposed Amended Rule 1134 Working Group #3

June 13, 2018

# Agenda

- Summary of previous working group meeting
- Continue BARCT analysis
  - ▷ Technology assessment
  - ▷ Establishing BARCT emission limit
  - ▷ Cost-effectiveness
- Rule concepts

## Previous Working Group Meeting

- Presented initial BARCT analysis
  - ▷ Identified emission levels of existing units
  - ▷ Assessed other rules and BACT determinations
- Provided initial rule concepts for Applicability, Emission Limits, and Exemptions

# BARCT Analysis

# BARCT Analysis Approach for PAR 1134

*Identify Emission Levels of Existing Units*

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graph TD; A[Identify Emission Levels of Existing Units] --> B[Assess Rules in Other Air Districts Regulating Same Equipment]; B --> C[Technology Assessment]; C --> D[Establishing the BARCT Emission Limit and Other Considerations]; D --> E[Cost-Effectiveness];
```

*Assess Rules in Other Air Districts Regulating Same Equipment*

Technology Assessment

Establishing the BARCT Emission Limit and Other Considerations

Cost-Effectiveness

# Technology Assessment

# Overview of Technology Assessment

Assessment of  
SCAQMD  
Regulatory  
Requirements

Assessment of  
Emission  
Limits for  
Existing Units

Other  
Regulatory  
Requirements

Assessment of  
Pollution  
Control  
Technologies

# Background

- Purpose of technology assessment is to assess current NOx control technologies for turbines
- Various sources researched to determine technological feasibility for NOx controls for turbines
  - ▷ Scientific literature
  - ▷ Vendor information
  - ▷ Strategies utilized in practice to achieve low NOx emissions
- Three major strategies identified to reduce NOx emissions from gas turbines
  - ▷ Combustion alteration
    - ▷ Steam/water injection
    - ▷ Lean premixed combustion
  - ▷ Exhaust controls
    - ▷ Selective Catalytic Reduction



# Steam/Water Injection

- Injection of water or steam into the high temperature flame zone
  - ▷ Lowers combustion zone temperature
  - ▷ Reduces NOx levels to approximately
    - ▷ 25 ppm for natural gas; and
    - ▷ 42 ppm for liquid distillate fuels
  - ▷ Imprecise application leads to some hot zones so NOx is still created
- Added water or steam increases mass flow through turbine creating a small amount of additional power

Control to  
25 ppm

# Lean Premixed Combustion

- Gaseous fuel and compressed air are pre-mixed minimizing localized hot spots that create high levels of NOx
  - ▶ Single digit (< 9 ppm) NOx emissions have been demonstrated on natural gas and landfill gas turbines with no SCR
  - ▶ Not available for liquid fuel turbines
- Requires that the combustor becomes an intrinsic part of the turbine design
  - ▶ Not available as a “retrofit” technology; must be designed for each turbine application

Control to  
9 ppm

# Selective Catalytic Reduction

- Primary post-combustion technology for NOx reduction<sup>1</sup>
  - ▷ Used in turbines, boilers, internal combustion engines (including heavy duty trucks), and other NOx generating equipment
  - ▷ Ammonia is injected into flue gas and reacts with NOx
  - ▷ Metal-based catalyst increases the reaction rate of NOx reduction
  - ▷ 80 to 90%+ reduction (reduces NOx levels to 2-5 ppm)
  - ▷ Improved reductions where mixture of NOx and ammonia is uniform
  - ▷ System susceptible to “poisoning” if flue gas contains contaminants (siloxanes, sulfur compounds, etc.)
- May be used in conjunction with combustion alteration NOx control technologies

Control to  
2 - 5 ppm

1. [https://www.epa.gov/sites/production/files/2017-12/documents/scrcostmanualchapter7thedition\\_2016revisions2017.pdf](https://www.epa.gov/sites/production/files/2017-12/documents/scrcostmanualchapter7thedition_2016revisions2017.pdf)

## Selective Catalytic Reduction (*continued*)

- Facilities may be space constrained to add more catalyst modules
- Environmental trade-offs
  - ▷ Pure anhydrous ammonia is extremely toxic and no new permits issued
  - ▷ Aqueous ammonia is somewhat safer but requires vaporization of water
  - ▷ Urea is safer to store, but requires conversion to be used
  - ▷ All have the potential for ammonia slip where unreacted ammonia is emitted from control device



# Other NOx Reduction Technologies

- Catalytic Combustion<sup>1</sup>
  - ▷ Lean premixed flameless combustion
  - ▷ On-going long-term testing indicates NOx levels below 3 ppm without SCR
    - ▷ Turbines with catalytic combustion are entering commercial market
  - ▷ Only available for replacement as it must be designed specifically for each turbine type
- Catalytic Absorption Systems<sup>2</sup>
  - ▷ Catalytic conversion of NOx with absorption/regenerative process
  - ▷ Similar NOx reduction potential as SCR (80-90% reduction; reduces NOx levels to 3-5 ppm)
  - ▷ Eliminates need for ammonia
  - ▷ High capital costs, complex system, high on-going costs, and regeneration issues remain

<sup>1</sup> <https://www.energy.gov/eere/amo/catalytic-combustion>

<sup>2</sup> [https://www.epa.gov/sites/production/files/2015-07/documents/catalog\\_of\\_chp\\_technologies\\_section\\_3.technology\\_characterization\\_-\\_combustion\\_turbines.pdf](https://www.epa.gov/sites/production/files/2015-07/documents/catalog_of_chp_technologies_section_3.technology_characterization_-_combustion_turbines.pdf)

# Summary of Primary NOx Control Technologies

Control Technique	NOx Levels (ppm)
Steam/Water Injection	25
Lean Premixed Combustion	9
Selective Catalytic Reduction	2 - 5
Lean Premixed Combustion and Selective Catalytic Reduction	2
Lean Premixed Combustion and Selective Catalytic Reduction	2

# BARCT Analysis Approach for PAR 1134

*Identify Emission Levels of Existing Units*

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*Assess Rules in Other Air Districts Regulating Same Equipment*

Technology Assessment

Establishing the BARCT Emission Limit and Other Considerations

Cost-Effectiveness

# Establishing the BARCT Limit



## Establishing the BARCT Limit

- Recommended BARCT limits are established using information gathered from:
  - ▷ Existing units
  - ▷ Other regulatory requirements
  - ▷ BACT requirements
  - ▷ Technology assessment

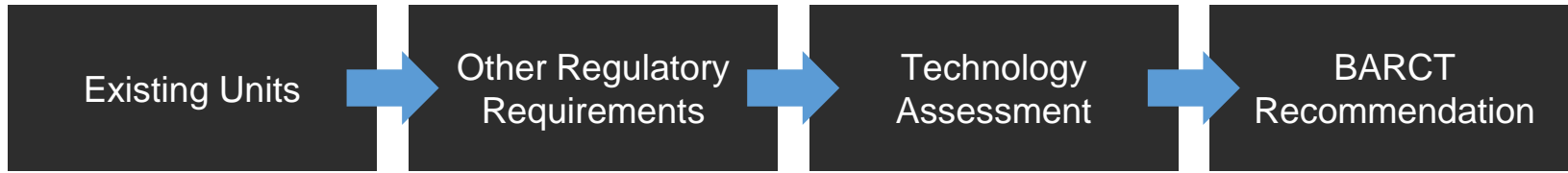
# Simple Cycle Natural Gas Turbines



<b>Retrofit</b>		5-25 ppm*	2.5 ppm	2.5 ppm
<b>New Install</b>	2.5 ppm	2.5-25 ppm*	2.5 ppm	2.5 ppm

\* Limit dependent on capacity

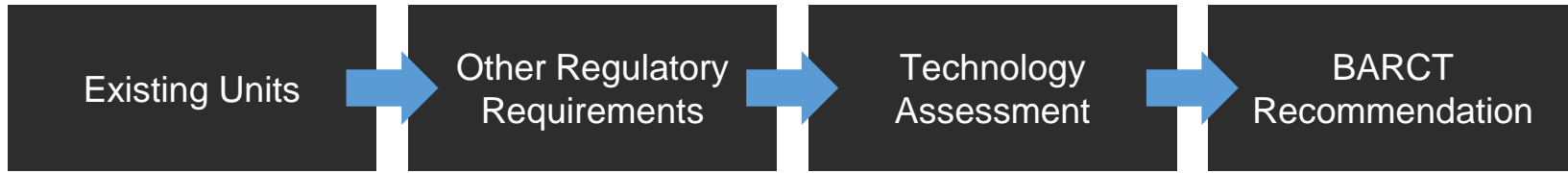
# Combined Cycle Natural Gas Turbines



<b>Retrofit</b>		5-25 ppm*	2.0 ppm	2.0 ppm
<b>New Install</b>	2.0 ppm	2.0-25 ppm*	2.0 ppm	2.0 ppm

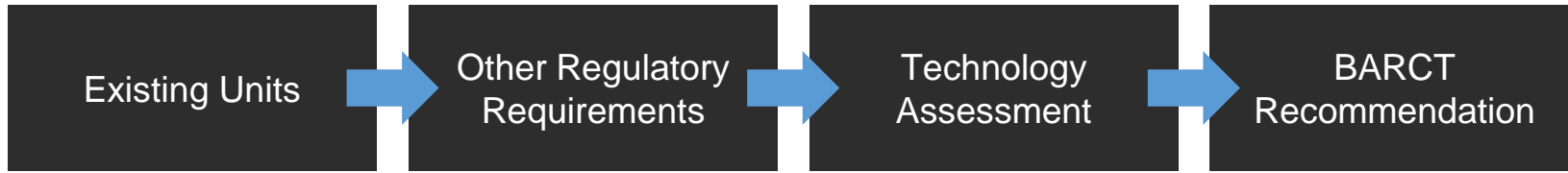
\* Limit dependent on capacity

# Landfill Gas Turbines



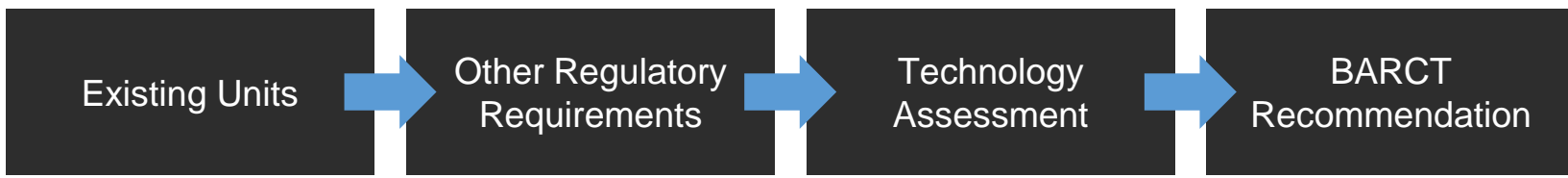
<b>Retrofit</b>		50 ppm	25 ppm	25 ppm
<b>New Install</b>	12.5 ppm	50 ppm	12.5 ppm	12.5 ppm

# Sewage Digester Gas Turbines



<b>Retrofit</b>	18.8 ppm	50 ppm	18.8 ppm	18.8 ppm
<b>New Install</b>		50 ppm	15 ppm	15 ppm

# Process Gas Turbines



<b>Retrofit</b>		50 ppm		
<b>New Install</b>	5 to 9 ppm	50 ppm	5 ppm	5 to 9 ppm

# BARCT Recommendation

- Based on technology assessment, other air district regulations, and BACT requirements, the following limits are technically feasible
  - Limits may be met by retrofit or replacement

<b>Turbine Type</b>	<b>NOx Limit (ppm @ 15% O2)</b>
Natural Gas	
Combined Cycle	2.0
Simple Cycle	2.5
Landfill Gas	12.5
Sewage Digester Gas	18.8
Process Gas	5.0

# BARCT Analysis Approach for PAR 1134

*Identify Emission Levels of Existing Units*

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*Assess Rules in Other Air Districts Regulating Same Equipment*

Technology Assessment

Establishing the BARCT Emission Limit and Other Considerations

Cost-Effectiveness



# Cost-Effectiveness

# Cost-Effectiveness

- Cost-effectiveness is a cost-benefit analysis comparing relative costs and outcomes
- It is measured in cost per ton of pollutant reduced
- SCAQMD uses Discounted Cash Flow Method to calculate cost-effectiveness
  - ▷ Cost-Effectiveness = Present Value/Emissions Reduced Over Equipment Life
  - ▷ Present Value = Capital Costs + (Annual Operating Costs \* Present Value Formula)
  - ▷ Present Value Formula =  $(1 - 1/(1 + r)^n) / r$ 
    - $r = (i - f) / (1 + f)$
    - $i$  = nominal interest rate
    - $f$  = inflation rate

# Cost Estimates for Natural Gas Turbines

- Using U.S. EPA's Air Pollution Control Cost Estimation Spreadsheet for Selective Catalytic Reduction<sup>1</sup> to determine retrofit costs
  - ▷ Methodology based on U.S. EPA Clean Air Markets Division Integrated Planning Model
  - ▷ Size and costs of SCR based on size, fuel burned, NOx removal efficiency, reagent consumption rate, and catalyst costs
  - ▷ Capital costs annualized over 25 years at 4% interest rate
  - ▷ 2015 annual reported emissions used to estimate annual MW output
  - ▷ Values reported in 2015 dollars
- Turbine replacement costs are \$1.2 million to \$3.3 million per MW<sup>2</sup> (2015 dollars)
- Stakeholders are welcome to provide staff with their own costs and cost-effectiveness calculations

1 - Available at: [https://www.epa.gov/sites/production/files/2017-12/documents/scrcostmanualchapter7thedition\\_2016revisions2017.pdf](https://www.epa.gov/sites/production/files/2017-12/documents/scrcostmanualchapter7thedition_2016revisions2017.pdf)

2 - Available at: [https://www.epa.gov/sites/production/files/2015-07/documents/catalog\\_of\\_chp\\_technologies.pdf](https://www.epa.gov/sites/production/files/2015-07/documents/catalog_of_chp_technologies.pdf)

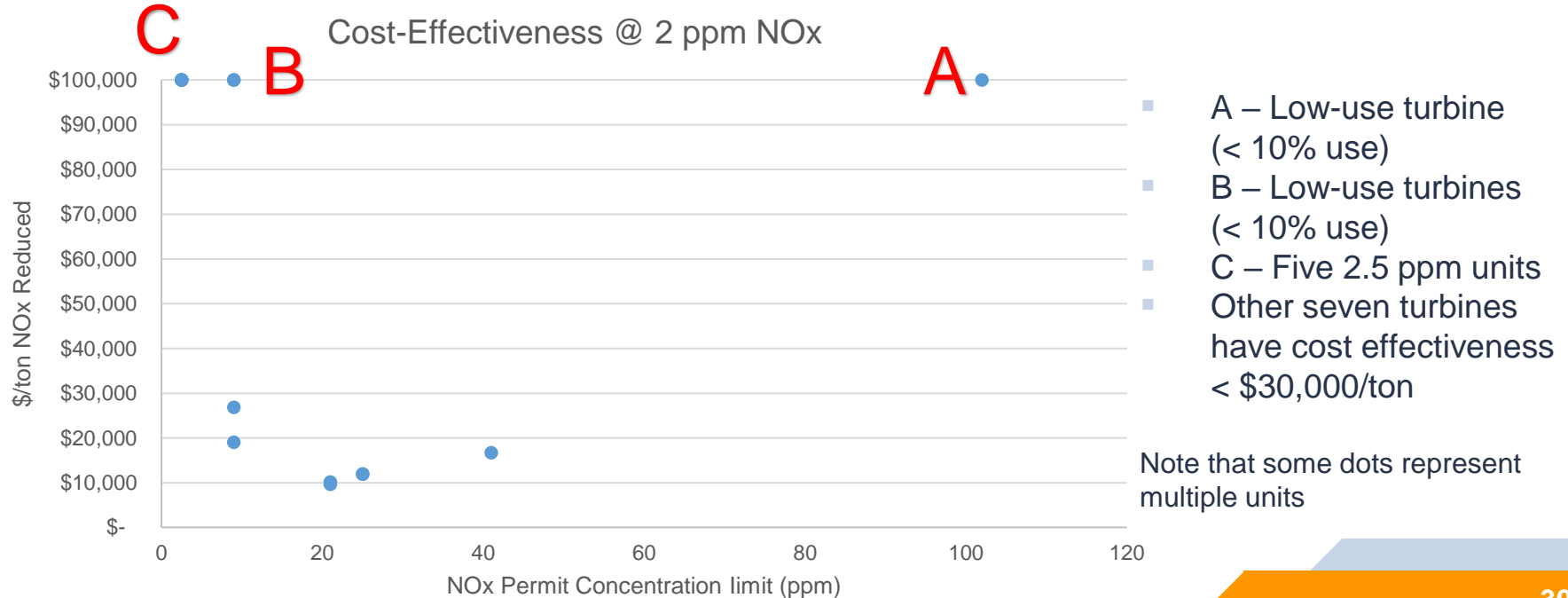
## Estimated Emissions Inventory and Reductions

- Baseline Emissions determined by using reported fuel consumption and permitted emission limit
- PAR 1134 Emissions determined by using reported fuel consumption and proposed emission limit
- Emission reductions are the difference between Baseline Emissions and PAR 1134 Emissions

# Evaluation of Cost-Effectiveness for Natural Gas Turbines

- Evaluated cost-effectiveness for all PAR 1134 turbines at the following proposed NO<sub>x</sub> concentration limits:
  - ▷ Combined cycle: 2.0 ppm
  - ▷ Simple cycle: 2.5 ppm
- Used 2015 emission data and costs
- Cost-effectiveness evaluation based on retrofit costs using U.S. EPA's Air Pollution Control Cost Estimation Spreadsheet for Selective Catalytic Reduction

# Combined Cycle Natural Gas Turbines

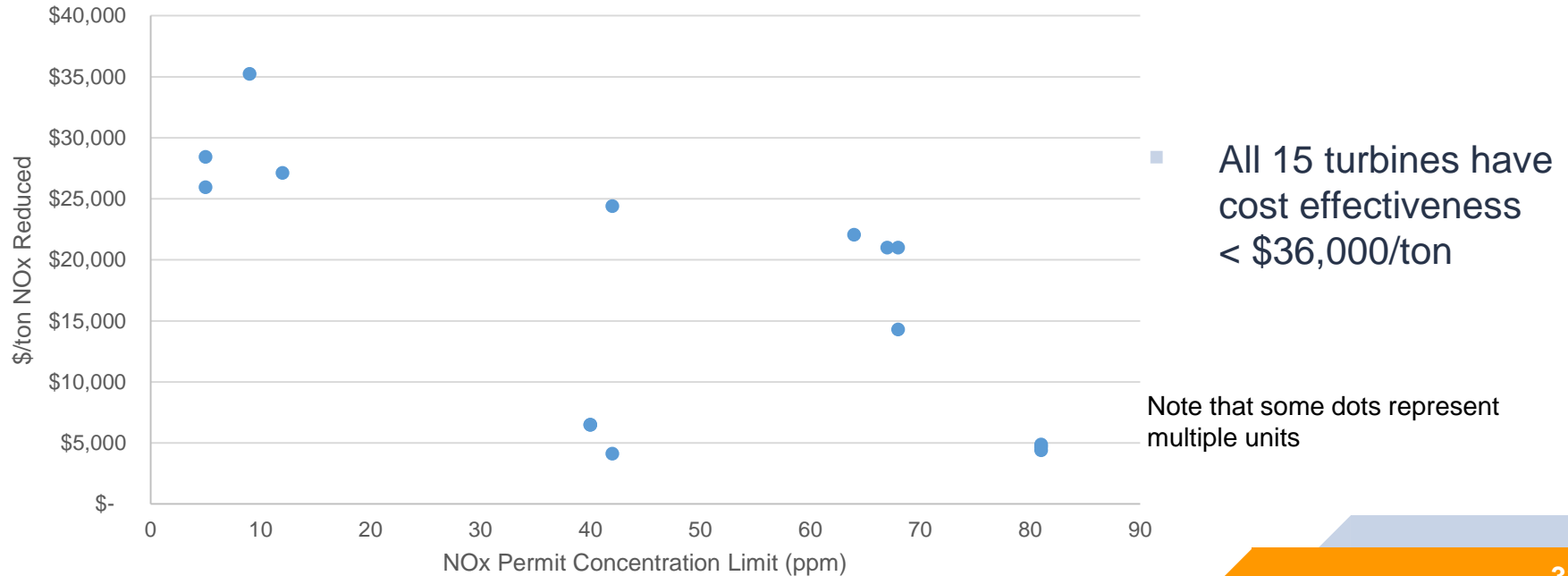


## BARCT Determination for Combined Cycle Natural Gas Turbines

- Proposed limit of 2.0 ppm cost effective for remaining seven units
  - ▷ Average cost effectiveness (excluding low-use and 2.5 ppm units) is approximately \$15,200/ton reduced
  - ▷ Highest cost effectiveness (excluding low-use and 2.5 ppm units) is approximately \$26,900/ton reduced
- Proposed limit of 2.0 ppm not cost effective ( $>$  \$100,000/ton reduced) for:
  - ▷ Low-use units utilized  $<$  10% of capacity
  - ▷ Turbines currently permitted at 2.5 ppm NO<sub>x</sub>

# Simple Cycle Natural Gas Turbines

Cost Effectiveness @ 2.5 ppm





## BARCT Determination for Simple Cycle Natural Gas Turbines

- Proposed limit of 2.5 ppm cost effective all 15 units
  - ▶ Average cost effectiveness is approximately \$16,800/ton reduced
  - ▶ Highest cost effectiveness is approximately \$35,300/ton reduced

# Natural Gas Pipeline Turbines

- Four < 1 MW turbines used for natural gas pipelines
  - ▷ Challenged by variation in fuel flow
  - ▷ Currently emitting < 10 tons combined annually
- BACT and SJVAPCD limits are currently 8 ppm steady and 12 ppm transition
- Analyzing technical feasibility and incremental cost-effectiveness to meet 2.5 ppm limit
  - ▷ BACT/SJVAPCD limit would result in approximately one ton of NOx emission reductions foregone annually

## Cost-Effectiveness for Landfill Gas Turbines

- Based on recent source testing, 12 of 16 landfill gas turbines can meet 12.5 ppm NO<sub>x</sub> limit
  - ▷ Considerations may be necessary for short periods where low loads or other permit restriction impact NO<sub>x</sub> emission concentrations
- Remaining four units installed in 2007 already using SCR control technology
  - ▷ Recent test results indicate that meeting 25 ppm permit limit is challenging
  - ▷ Experiencing high costs due to frequent catalyst replacement
- More recent version of turbine model reportedly has NO<sub>x</sub> emissions of 15 ppm with no SCR
  - ▷ Stranded assets may be somewhat offset by elimination of SCR control costs
  - ▷ Estimated cost effectiveness for replacement is \$42,000 per ton (45 tons reduced); without stranded assets cost effectiveness is \$30,100 per ton
  - ▷ If significant changes to filters, piping, etc. are required then cost effectiveness is approximately \$82,000 per ton

## Sewage Digester Gas Turbines (Retrofit)

- Three turbines currently meet 18.8 ppm NO<sub>x</sub> using SCR
- Examining cost for other three turbines to meet same limit
- In addition to SCR costs, filtering costs to remove contaminants
  - ▷ Filtering capital costs range from \$1.0 to \$7.1 million<sup>1</sup>
  - ▷ Annual filtering operation and maintenance costs range from \$0.3 to \$1.1 million<sup>1</sup>
  - ▷ Estimated 23.2 tons of NO<sub>x</sub> reduced annually from all four turbines

<sup>1</sup> – GTI Technical – Final Report AQMD Contract #: 13432; Conduct a Nationwide Survey of Biogas Cleanup Technologies and Costs

# Sewage Digester Gas Turbines (Replacement)

- Recent version of model installed in early 2000's reportedly has NOx emissions of 15 ppm with no SCR
  - ▷ Lean combustion control produces less NOx than steam injection control
  - ▷ Some loss of power from steam removal
  - ▷ If loss of power doesn't impact operations, then cost impacts may be insignificant
  - ▷ If larger units required to make up for lost power, then significant changes may be necessary for piping, filtering, housing, etc.
  - ▷ Estimated 46 tons of NOx reduced from all four turbines

## Process Gas Turbine

- Six offshore platform process gas turbines to be replaced
  - ▷ Plans are to replace three by electrification and three with new turbines
  - ▷ New turbines will be subject to BACT
  - ▷ Turbines utilize diesel fuel as back-up to process gas
    - ▷ Diesel fuel allowed only when there is no access to natural gas
  - ▷ Considering 5 to 9 ppm limit for process gas and 25 ppm limit for liquid fuel

# Incremental Cost for Offshore Platform Process Gas Turbines

- Differential cost effectiveness between new turbine purchase and new turbine purchase with SCR control
  - ▷ Estimated capital cost of new turbines = \$16.5 million (\$5.5 million each)
  - ▷ Estimated capital cost of SCR = \$2.7 million (\$0.9 million each)
  - ▷ Estimated annual costs for SCR = \$0.2 million
  - ▷ Estimated emission reduction without SCR (9 ppm) = 18.5 tons
  - ▷ Estimated annual emission reductions with SCR @ 5 ppm = 18.8 tons
- Cost effectiveness of new turbines = \$36,000 per ton of NOx reduced
- Cost effectiveness of new turbines with SCR = \$48,000 per ton of NOx reduced
- Incremental cost effectiveness > \$800,000 per ton

# BARCT Analysis Summary

Gas Turbine Fuel	Proposed Limit (ppmv @ 15% O <sub>2</sub> )	Cost-Effectiveness (cost per ton of NO <sub>x</sub> reduced)
Natural Gas		
Simple Cycle	2.5	\$16,800
Combined Cycle	2.0	\$15,200
Landfill Gas	12.5	\$42,000 to \$82,000
Sewage Digester Gas	18.8	Still assessing costs
Process Gas	5 – 9 (25 for liquid fuel)	\$36,000 to \$48,000



# Rule Concepts

# Rule Concepts – *Emission Limits*

Gas Turbine Fuel	Proposed Limit (ppmv @ 15% O <sub>2</sub> )
Natural Gas	
Simple Cycle	2.5
Combined Cycle	2.0
Landfill Gas	12.5
Sewage Digester Gas	18.8
Process Gas	5 – 9 (25 for liquid fuel)

- Limits averaged over one hour
  - ▷ Explore longer averaging period for sewage digester gas turbines
- Effective date January 1, 2024
- Considering replacement requirement for turbines older than 25 to 35 years

## Rule Concepts – *Monitoring*

Monitoring is critical to ensure equipment is operating properly

- Retain continuous emission monitoring system for units  $\geq 2.9$  MW
- New requirements for monitoring
  - ▷ Update Continuous Emission Monitoring Systems (CEMS) Requirements Document for Utility Boilers
  - ▷ Relative Accuracy Test Audit (RATA) annually
  - ▷ Relative Accuracy Audit (RAA) quarterly
  - ▷ Daily calibration
  - ▷ Missing data procedures for up to 72 hours in any one calendar month
  - ▷ Remove monitoring requirements for volumetric flow, heat input rate, and net MWH produced
  - ▷ Add monitoring requirements for ammonia

# Rule Concepts – Data Acquisition

- Data acquisition system requirements
  - ▷ NO<sub>x</sub> emission rate (ppm)
  - ▷ O<sub>2</sub> concentration (ppm)
  - ▷ Ammonia (ppm)

## Rule Concepts – *Source Testing*

- **Current requirements**
  - ▷ Annual source testing if unit emits more than 25 tons annually
  - ▷ Otherwise within 90 days after 8,400 hours of operation
- **Proposed requirements**
  - ▷ Source testing every three years only if RATA not applicable

## Rule Concepts – *Recordkeeping and Reporting*

- Current requirements
  - ▷ Records maintained for two years
  - ▷ Monthly reporting of emissions
  - ▷ RECLAIM requirements
- Proposed Requirements
  - ▷ Require records maintained and made available upon request for five years

# Schedule

## Current Tentative Schedule

- Next Working Group Meeting July 2018
- Public Workshop Summer 2018
- Stationary Source Committee Fall, 2018
- Set Hearing Fall 2018
- Public Hearing Fall 2018



# Contacts

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